# Biobased acrylic acid production through Reheterogeneous catalysis: towards process



# electrification ECE25 CION





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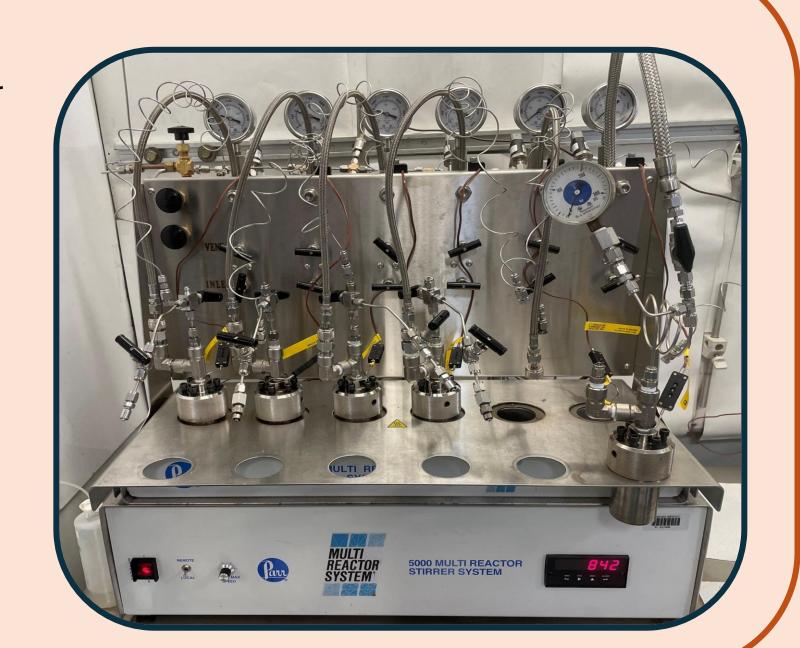
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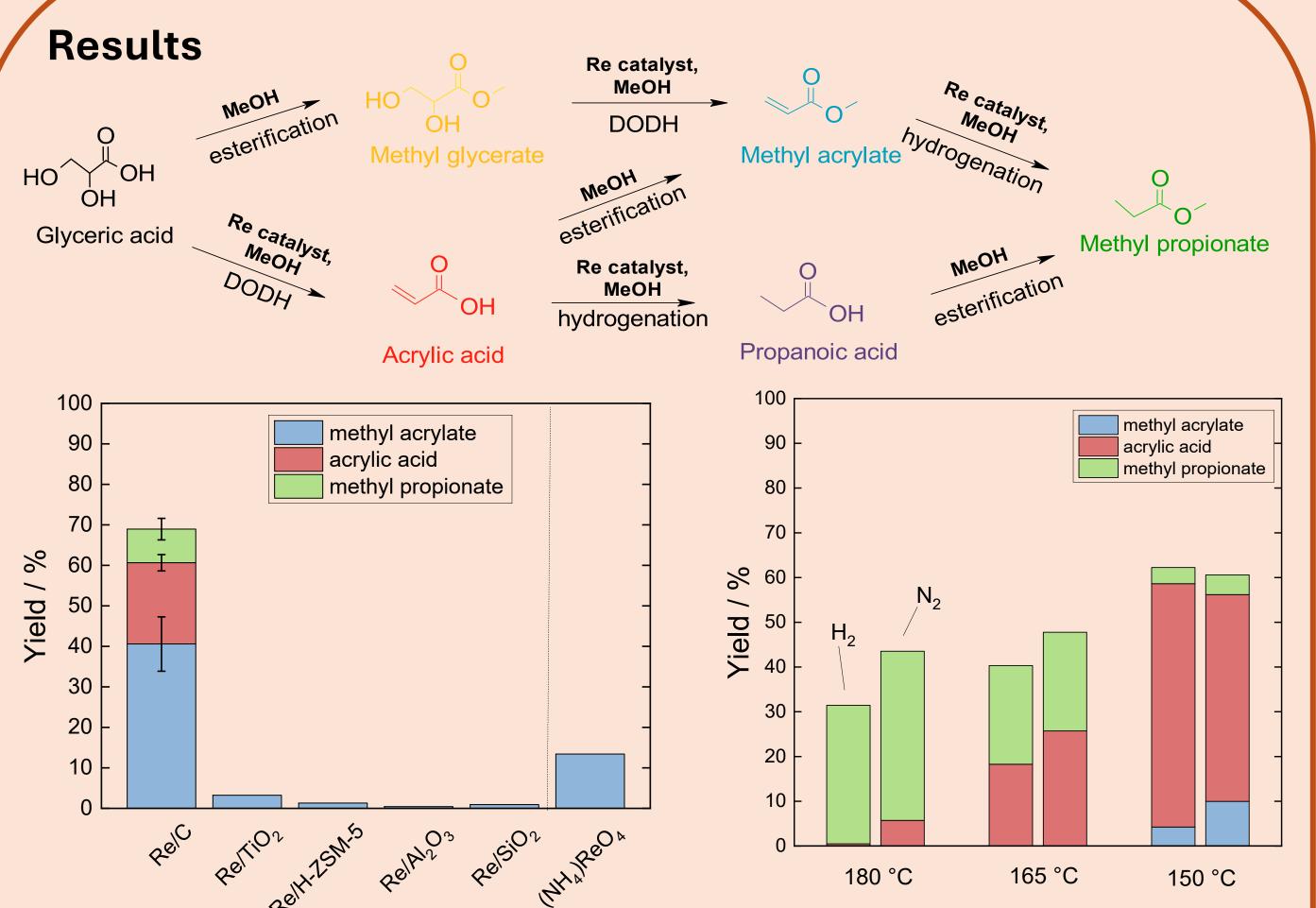
#### Introduction

Biomass-to-value-added-product routes often rely on the catalytic removal of oxygen from feedstock using  $H_2$  over supported metal catalysts, with recent attention focused on Re-catalyzed deoxydehydration (DODH). A notable example is the also catalytic route using a Re/C catalyst to convert glyceric acid to acrylic acid and its esters, which are highly sought-after chemical building blocks, especially for polymer production In the study we explored different supported Re catalysts regarding their catalytic behavior for DODH of glyceric acid. <sup>1</sup>

#### **Methods**

- High pressure stainless stell reactor sistem with magnetic bar stirrer
- $V_{reactor} = 75 \text{ mL}$
- Temperature from 120 °C to 180 °C
- $5 \operatorname{bar}_{g} \operatorname{N}_{2} \operatorname{or} \operatorname{H}_{2}$
- 800 rpm of stirring speed
- m<sub>reactant</sub> = 100 mg of Glyceric acid
- m<sub>solvent</sub> = 35 g of MeOH
- m<sub>catalyst</sub> = 140 mg of different Rhenium base catalyst with 5 wt. % of Re loading
- GC-MS for analysis of the products



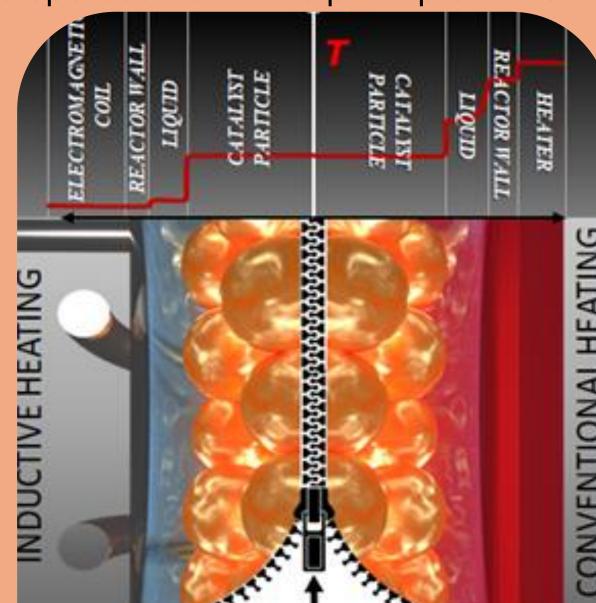


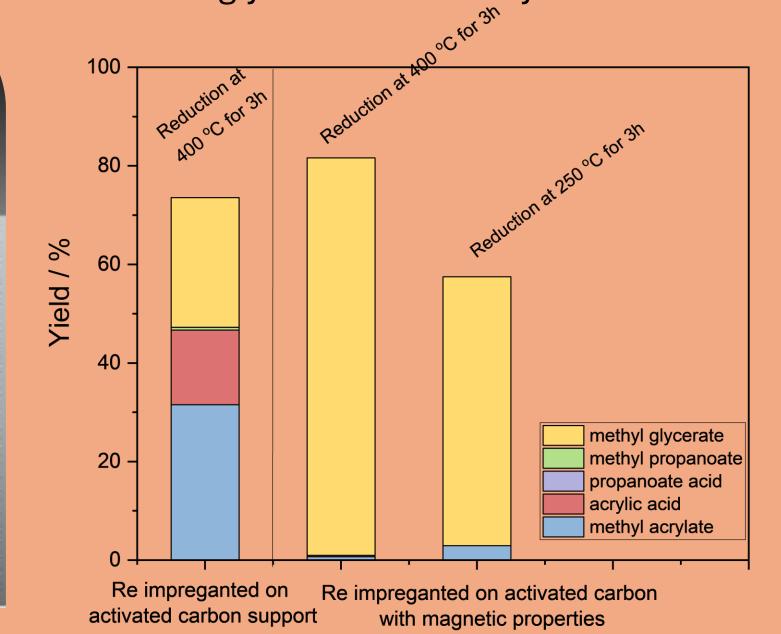
**Figure 1:** Yields of deoxydehydration products after 72 h over different supported Re catalysts in methanol at T = 150 °C, 5 bar<sub>g</sub>,  $N_2$  atmosphere.

**Figure 2:** Yields of deoxydehydration products after 72 h over Re/C in methanol at different temperature at 5 bar<sub>g</sub>  $N_2$  or  $H_2$  atmosphere.

# **ELECTRIFICATION OF REACTORS AND PROCESSES**

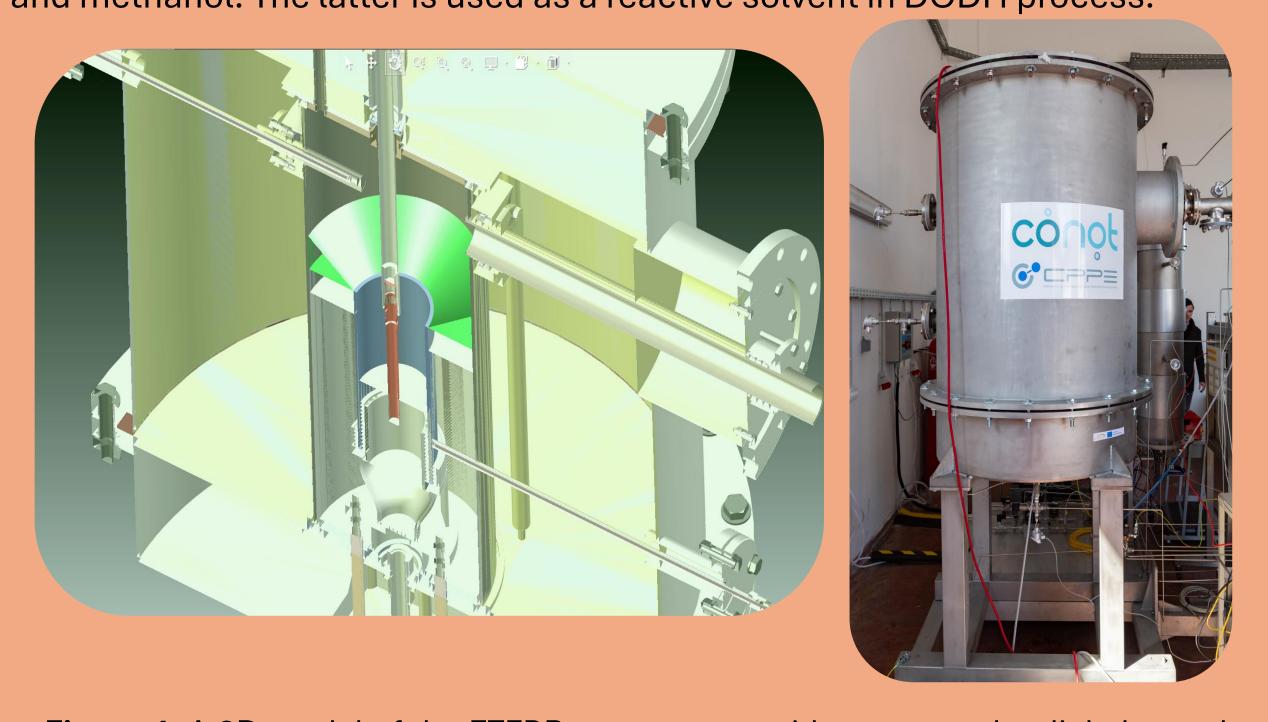
To overcome the problem of temperature gradients in the reactor and ultimately promote or inhibit bulk-phase reactions or the breakdown of thermally unstable compounds, the suspended solid phase (catalyst or heat-carrier) can be selectively heated by magnetic heating of magnetic particles (Figure 3)<sup>2</sup>. For magnetic heating showcase our research team has effectively synthesized and applied a catalyst with magnetic nanoparticles (MN) coated by carbon and finely dispersed Re for the principle in DODH of biobased glyceric acid to acrylic acid.





**Figure 3:** A schematic representation of a temperature profile in magnetic-and conductive-heated reactor<sup>2</sup> or electrified fluidized bed reactor and a comparison of Re-impregnated on commercial C-support with ferrimagnetic maghemite nanoparticles (MN), At T = 150 °C, 5 bar<sub>g</sub>, N<sub>2</sub> atmosphere.

Similarly, (catalyst) **particles can be heated directly** via electrical resistant heating, while electrical current flows through the conductive bed material fluidized by the gas stream as demonstrated in e-CODUCT project. The electrothermal-fluidized-bed-reactor (ETFBR) technology has been demonstrated on a pilot scale with 2 kg/h capacity in Slovenia. The pilot unit is designed to convert greenhouse gases (such as  $CO_2$ ) and acid gases (such us  $H_2S$ ) into sulfur and methanol. The latter is used as a reactive solvent in DODH process.



**Figure 4:** A 3D model of the ETFBR reactor core with center and radial electrodes clearly visible. Pilot reactor diameter is significantly larger (due to thermal insulation) then the fluidized-bed zone, as the latter is being heated upto 1200 C.

## Conclusion

- The commercial Re/C catalyst showed by far the highest catalytic activity (60.6% yield of methly acrylate and acrylic acid) of all catalysts tested with the most optimal condition: 150°C in methanol after 72 hours in N2
- Also magnetic catalyst showcased catalytic activity (5% yield)
- **Future work**: the catalyst will be tested in the batch induction-heated reactors to evaluate the activity, stability, selectivity under conditions that minimize transport limitations.
- **Electrification** of reactors and processes boosts the energy efficiency and flexibility of chemical processes.

### References

- 1 M. Gabrič, F. M. Harth, B. Hočevar, S. Gyergyek, B. Likozar and M. Grilc, Green Chemistry, 2025, 27, 3640-3645.
  - J.-S. Pavelić, S. Gyergyek, B. Likozar and M. Grilc, Chemical Engineering Journal, 2025, 505, 158928.

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