

Alternative to Claus process through COS as intermediate. Part 1: CO₂ and H₂S competitive adsorption on zeolite 13X

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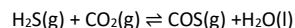
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Introduction

According to recent data, the largest share of carbon emissions per sector in 2021 came from producing electricity and heat, accounting for 40% of global CO₂ emissions, reaching a historic high of 14.6 Gt¹. In industrial-scale applications, fossil fuel combustion is commonly used to generate the heat required for chemical reactions. It is estimated that approximately half of the CO₂ emissions in the chemical industry are attributed to fuel combustion for heat supply purposes, where refineries and petrochemical industries are responsible for 1.24 Pty of CO₂ emissions. At the same time, this sector handles more than 3.6 Mt/y of H₂S, which in admixture with CO₂ is called acid gas and is handled not only in refining but also in exploration and production (as components of natural gas reservoirs), in biogas treatment (as natural components of the gas mixture from a digester), etc. The existing acid gas treatment approach relies on the Claus process to recover sulfur from gas streams rich in H₂S and demands additional use of fuel gas for lean H₂S sources (<55%). In contrast, thermo-catalytic or electrocatalytic CO₂ reduction and sequestration demand high purity of CO₂, requiring a proper separation from the acid gas. Moreover, to this date, no existing technologies allow simultaneous reduction of CO₂ and H₂S.

To address the transition to a low-carbon economy, the chemical industry needs to reduce its fossil fuel consumption by decarbonizing its processes, in particular through electrification. The project e-CODUCT provides a new technology for two-step acid gas valorization via i) conversion of CO₂ and H₂S into COS in a fixed bed reactor, following the reaction:



and ii) COS conversion into CO and SX using an electrothermal fluidized bed (ETFB) reactor. In this work, we address the first step (i) by studying the role of FAU- and LTA-type basic zeolites on the competitive adsorption and reaction of CO₂ and H₂S.

Materials and Methods

Adsorption and reaction of CO₂ and H₂S were performed at atmospheric pressure in a fixed-bed quartz reactor (9 mm diameter) at 45°C. The reactor was fed with a diluted mixture of H₂S (Linde, purity: 95%v in N₂) and CO₂ in nitrogen at different ratios (3-12%v) using a constant flow of 4.8 L/h (STP). Before testing, catalysts (13X and 4A zeolites from SGCREE, SAR=1.5 and 1.2, respectively) were compacted under 5 tons, crushed, and sieved to obtain homogenous particles (0.2-0.5 mm), then 4g were loaded in the reactor. Firstly, all samples were pre-treated at 350°C under nitrogen flow 1.8 L/h (STP) for 8-10 h.

Results and Discussion

Because of the low temperature, physisorption and chemisorption are discriminated through the saturation of the zeolite followed by a thermal desorption procedure. For both molecules, H₂S and CO₂ adsorbed separately on 13X, the amount is less than 10%, corresponding to an extremely low ratio with respect to the sodium cation (0.6 mol/g for 13X). Moreover, the strength of the adsorption of H₂S is higher than the CO₂, as witnessed by the higher desorption temperature, typically attributed to a dissociative adsorption mechanism on the sodium cation.^{2,3}

Table 1. Summary of adsorption results on 13X at 45°C (p=0.13).

molecule	Physisorbed (mmol/g)	Chemisorbed (mmol/g)	% chem.	T desorption (°C)
H ₂ S	2.95	0.21	6.7	330
CO ₂	1.44	0.14	9.0	125

The injection of CO₂ on the catalyst with previously chemisorbed H₂S produces COS and H₂O, the latter remaining adsorbed in the zeolite. The almost complete conversion of the chemisorbed H₂S suggests the importance of these species towards the COS formation. The same experiments are carried out with the reverse order of reagents. The co-adsorption and reactivity of H₂S and CO₂ are further characterized by *operando* infrared spectroscopy.

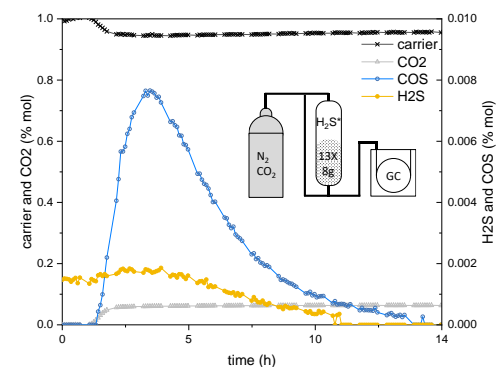


Figure 1. Reaction products from a continuous flow of CO₂ on previously chemisorbed H₂S.

Significance

We report a new route for Claus process defossilization with potential for industrial implementation.

References

1. The Paris Agreement UNFCCC, (May 2023), unfccc.int/process-and-meetings/the-paris-agreement
2. Yum et al, Separations **2022**, 9, 229.
3. Khabazipour et al., Ind. Eng. Chem. Res. **2019**, 58, 22133–22164.