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# eQATOR: Electrically heated catalytic reforming reactor

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# Project information

- June 2022 – November 2025
- Project budget 8.544 M€
- Project grant 7.536 M€



# Renewable carbon needed for green transition

- Energy can be *decarbonised*. Chemicals and materials must be *defossilized*.
  - Make chemicals and materials from renewable carbon sources rather than fossil carbon sources
  - CO<sub>2</sub>, biomass, recycled carbon materials (i.e., plastics)
- Biogas is an attractive source of renewable carbon
  - Ca. 50:50 mixture of CH<sub>4</sub> and CO<sub>2</sub>
  - Agricultural
  - Urban (organic fraction of municipal solid waste)
  - 35 Mtonne produced in 2018
  - Estimated growth 4.4 % p.a.
- Biogas currently used *only* for energy production
  - CH<sub>4</sub> separated, CO<sub>2</sub> emitted

**Utilization of biogas for chemicals production – specifically methanol (CH<sub>3</sub>OH or MeOH) via dry reforming – will defossilize some MeOH production and promote development of local MeOH economies.**

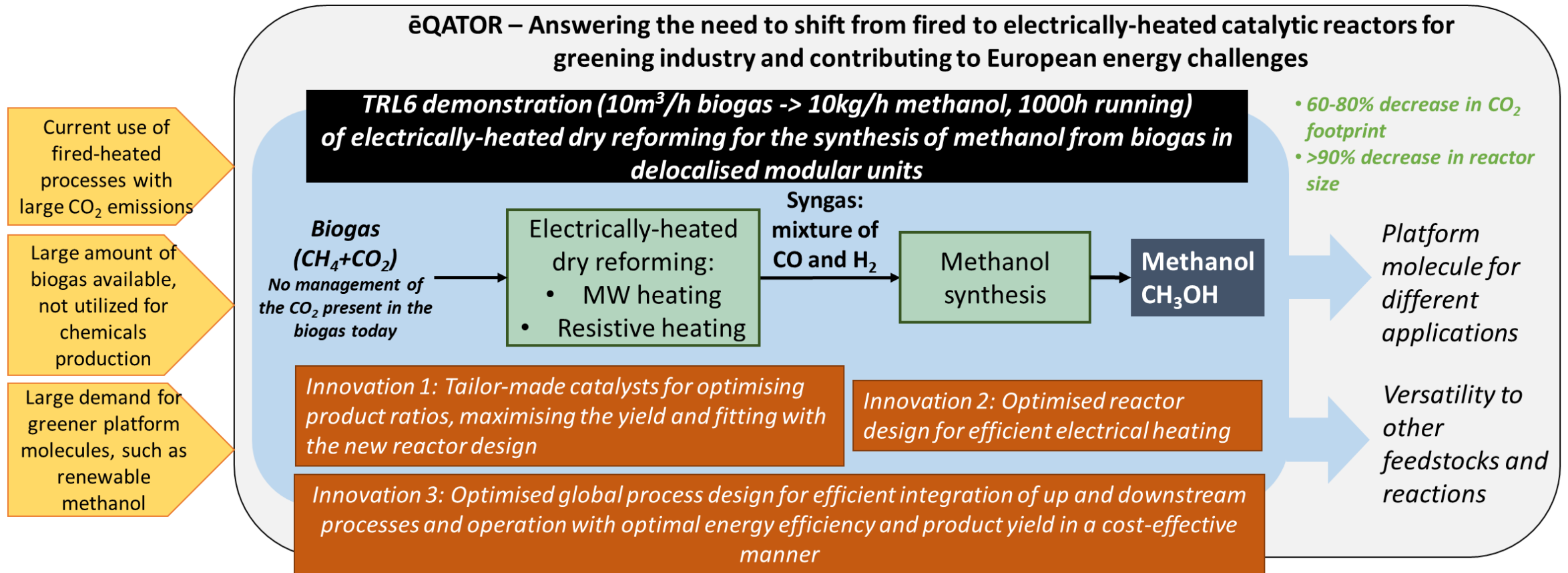


# MeOH production today

- MeOH is an important base chemical
  - Global market size ca. 98 Mtonne
  - Used as fuel, starting point for many chemicals and polymers
  - World class plants produce up to 3 Mtonne/a
- Production via steam reforming of natural gas to syngas (mixture of CO and H<sub>2</sub>), then syngas to MeOH
  - Fossil carbon is both the carbon feedstock and the energy source
  - Reactor heating produces 350 kg CO<sub>2</sub> per 1000 Nm<sup>3</sup> syngas
  - Product related emissions are 307 kg CO<sub>2</sub> per 1000 Nm<sup>3</sup> syngas
  - Emissions account for 10 % of the CO<sub>2</sub> emissions from the chemical sector
- About 0.2 Mtonne renewable MeOH produced/a
  - Primarily from CO<sub>2</sub> and H<sub>2</sub> (CCU approach)

# Project objectives

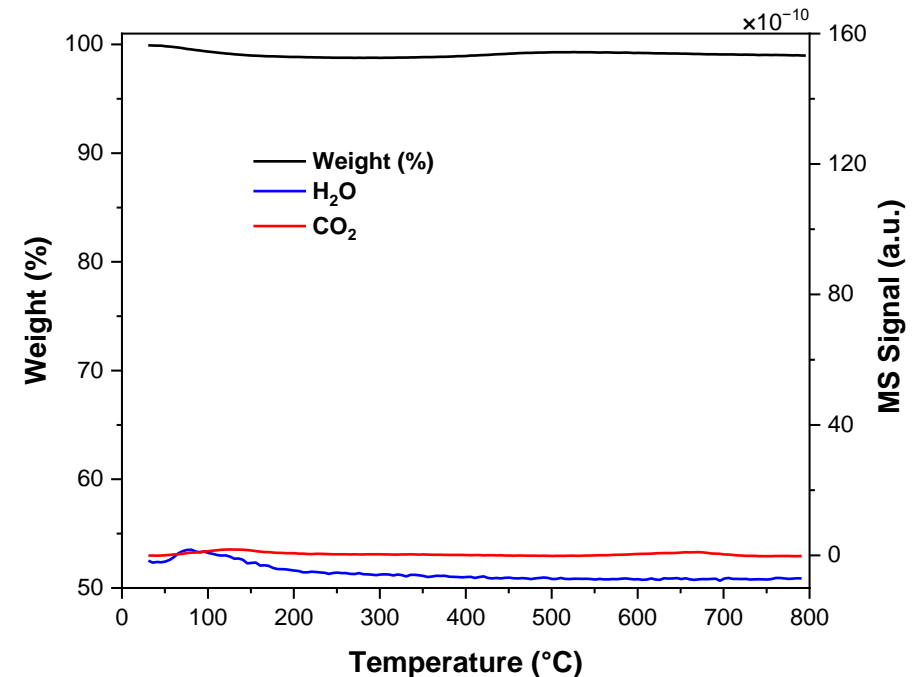
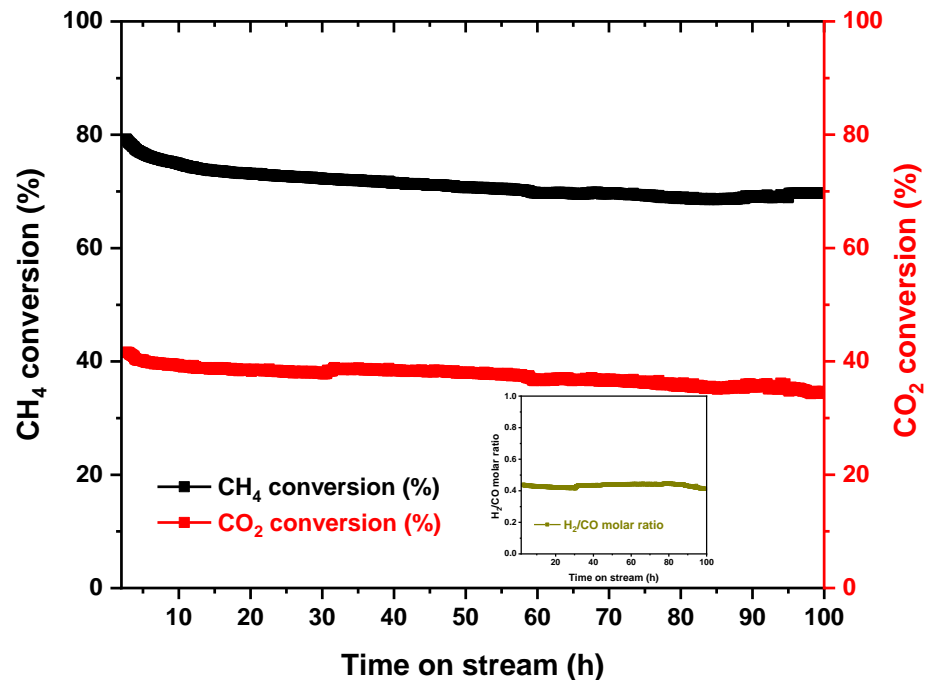
- Syngas from the dry reforming of methane ( $\text{CH}_4 + \text{CO}_2$ ), rather from steam reforming of methane
  - More difficult reaction, more prone to coking



- Current use of fired-heated processes with large CO<sub>2</sub> emissions
- Large amount of biogas available, not utilized for chemicals production
- Large demand for greener platform molecules, such as renewable methanol

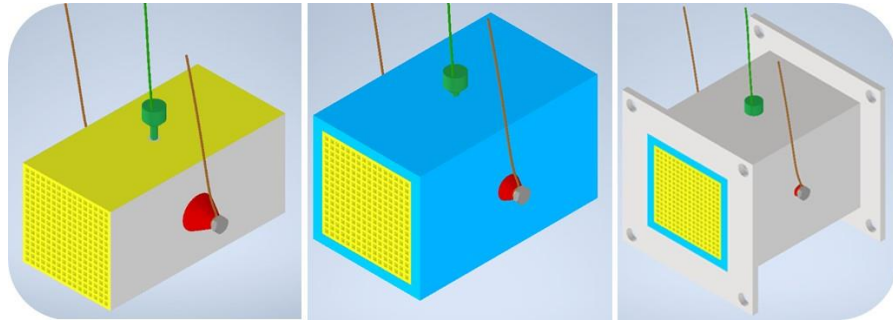
# Catalyst and process development

- Catalyst coking needs to be minimized/avoided
- Processes developed that provide gas mixtures with minimal coking potential
  - Dry Reforming ( $\text{CH}_4 + \text{CO}_2$ ) for a biogas composition produced from the organic fraction of municipal solid waste
  - Mixed Reforming ( $\text{CH}_4, \text{CO}_2, \text{H}_2\text{O}$ ) for a biogas composition produced from agricultural residues (manure)
- Catalyst composition found that shows minimal coking with the Dry Reforming gas mixture over 100 h





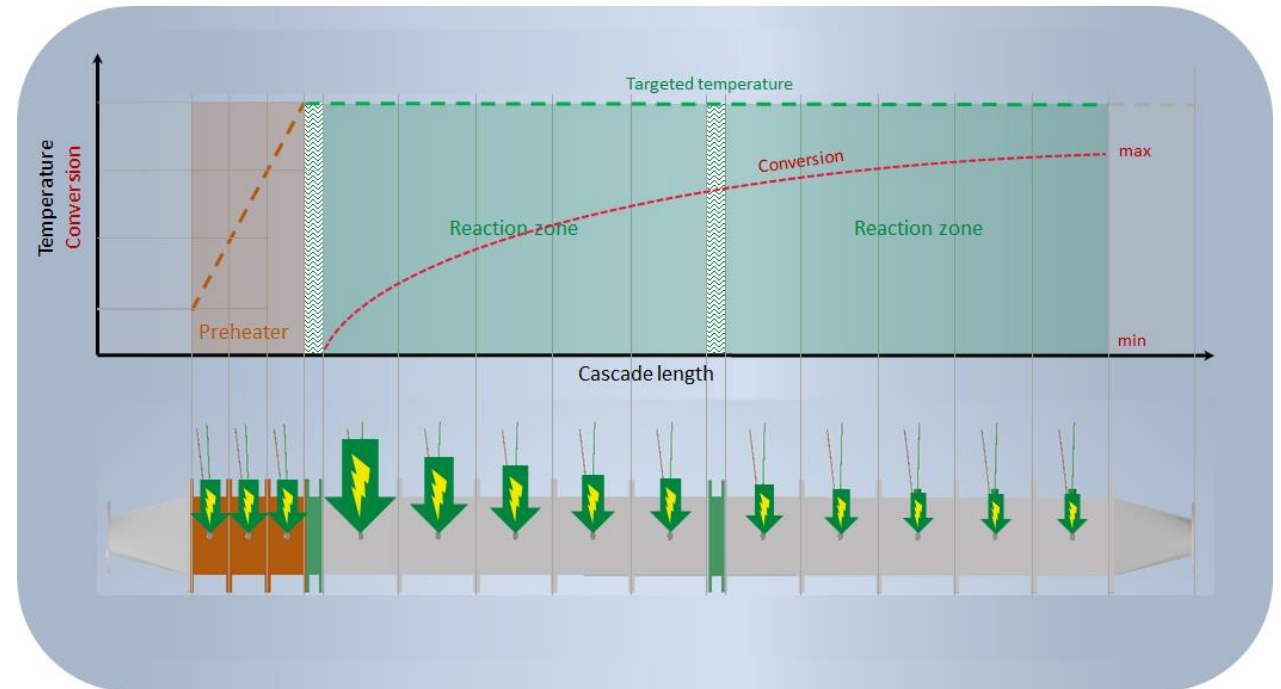
# Reactor development – resistive heating reactor



Coated honeycombs with electrodes, fiber mats, and metal housing

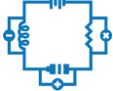



T = 1100 °C



Schematic temperature profile and conversion over cascade length – differentiated power supply possible

# Key Impacts

eQATOR provides an integrated development of catalysts and reactors, and two different, complementary electric heating technologies: **resistive heating**  and **microwave heating** 



**Reduction of carbon dioxide emissions by 60-80 %** compared to current syngas production processes. This reduction will **save from 7 Mt CO<sub>2</sub> per year in 2030, up to around 45 Mt CO<sub>2</sub> per year in 2045.**



**Higher conversion per pass**, improved heat management, **higher energy efficiency** and better carbon utilisation and atom economy, in **more compact reactors**, using renewable carbon feedstock.



**Strong industrial commitment** to reach widespread deployment of catalytic process electrification, through economically-viable, local, smaller-scale methanol production from biogas.



Novel, **optimised catalysts** and **reactor designs** for biogas valorisation to methanol.





# Pathway to TRL 9

- Project will reach TRL 6 by project end
  - Demonstration of resistive heating and microwave heating with two different gas mixtures
  - Dry Reforming (only CO<sub>2</sub> and CH<sub>4</sub>) and Mixed Reforming (CO<sub>2</sub>, CH<sub>4</sub>, H<sub>2</sub>O)
  - 10 Nm<sup>3</sup>/h feed for 1000 h
  - Methanol production step studied on modelled gas from syngas compositions
- Full-scale commercial plant anticipated to have feed of 500 Nm<sup>3</sup>/h
- TRL 6 reactor design and construction aims to be fully scalable
  - Material selection suitable for larger scale
  - Parallel reactor configuration
- Next step (given caveats of a successful project with positive economic and environmental outlook)
  - Combined reforming and MeOH production at ca. 100 Nm<sup>3</sup>/h scale



# Acknowledgements

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- eQATOR consortium



[www.eqator.eu](http://www.eqator.eu)



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