

Acid gas conversion to COS by Zeolite 13X: an elementary assessment

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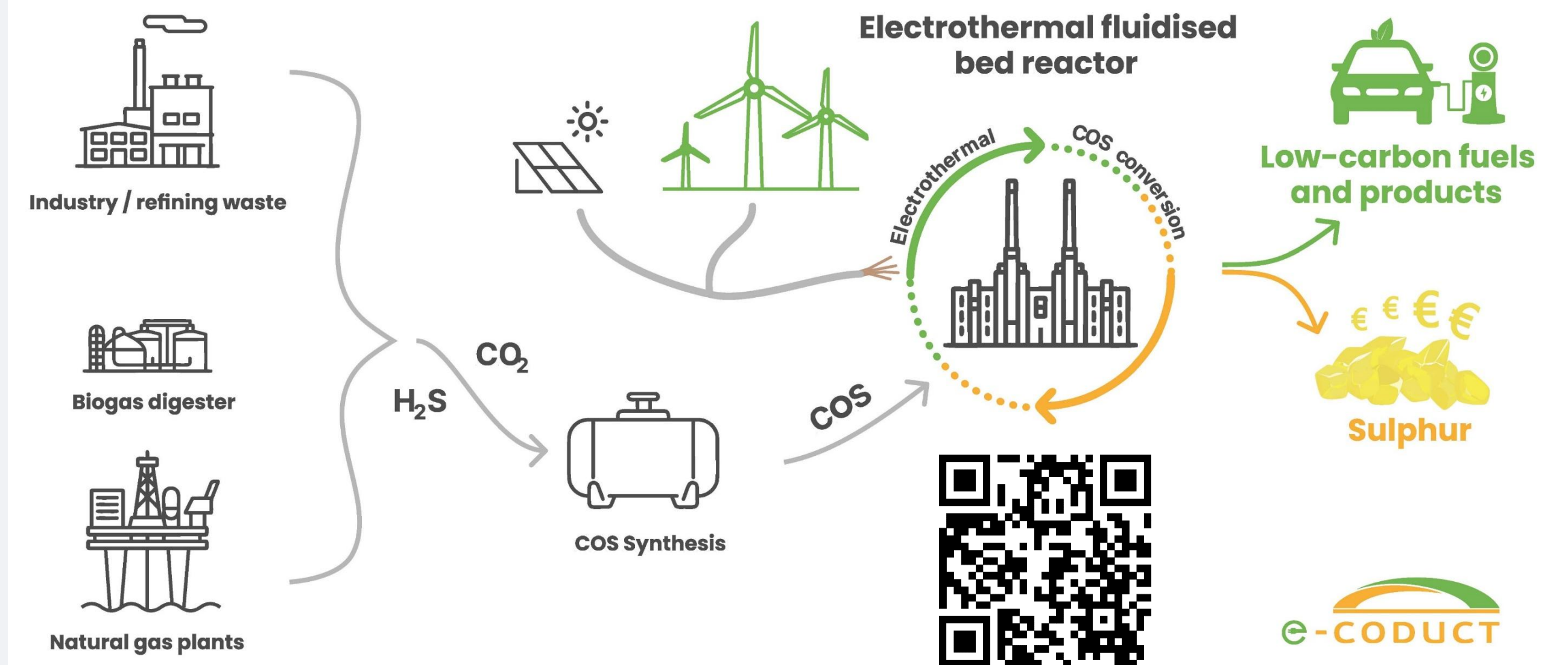
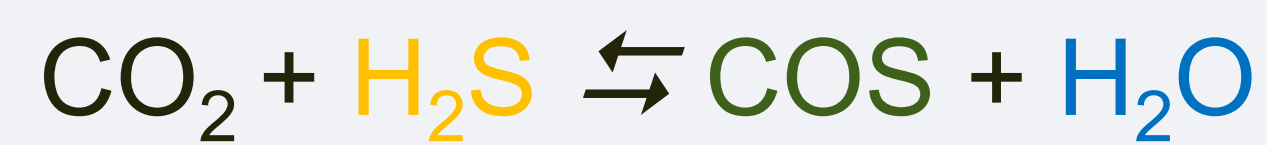
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INTRODUCTION

Current technologies for CO₂ conversion demand highly pure CO₂ feed streams, complicating the use of streams containing impurities such as H₂S. The e-CODUCT project focuses on developing an integrated approach for treating acid gas streams through a two-step process. First, COS is produced from CO₂ and H₂S using zeolite catalysts. Then, COS is decomposed in an electrothermal fluidized bed to yield CO, a valuable platform molecule, and marketable sulphur.

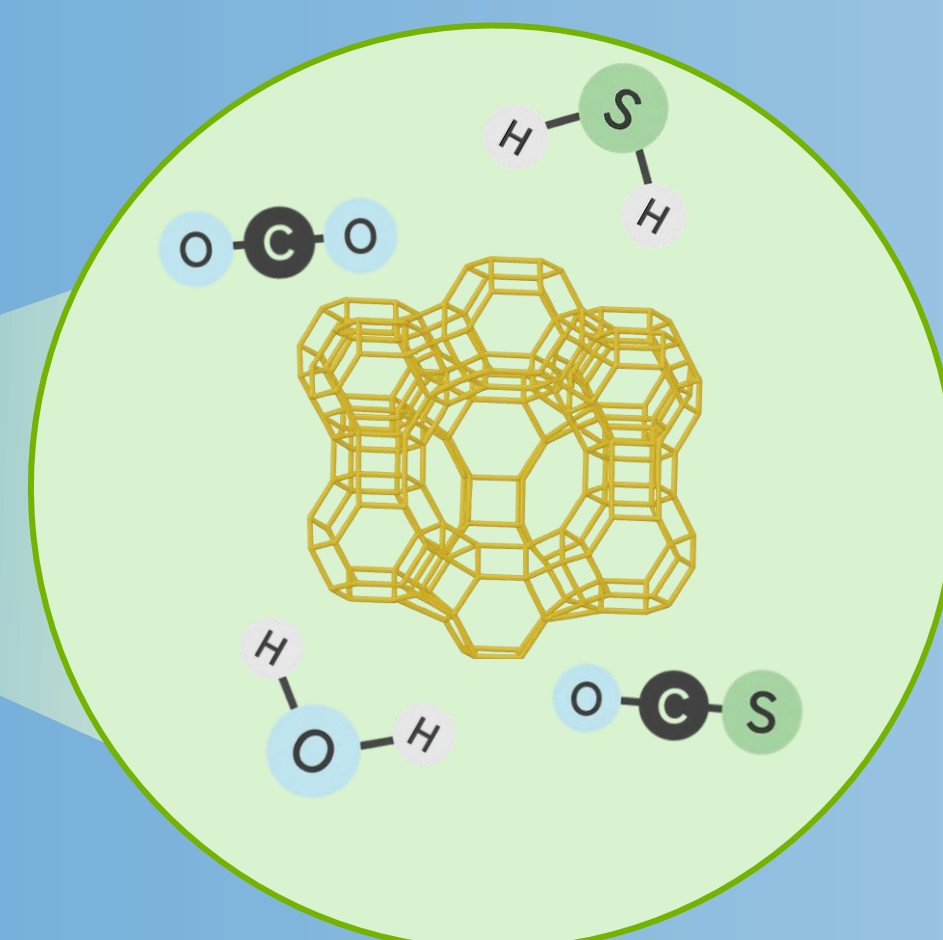
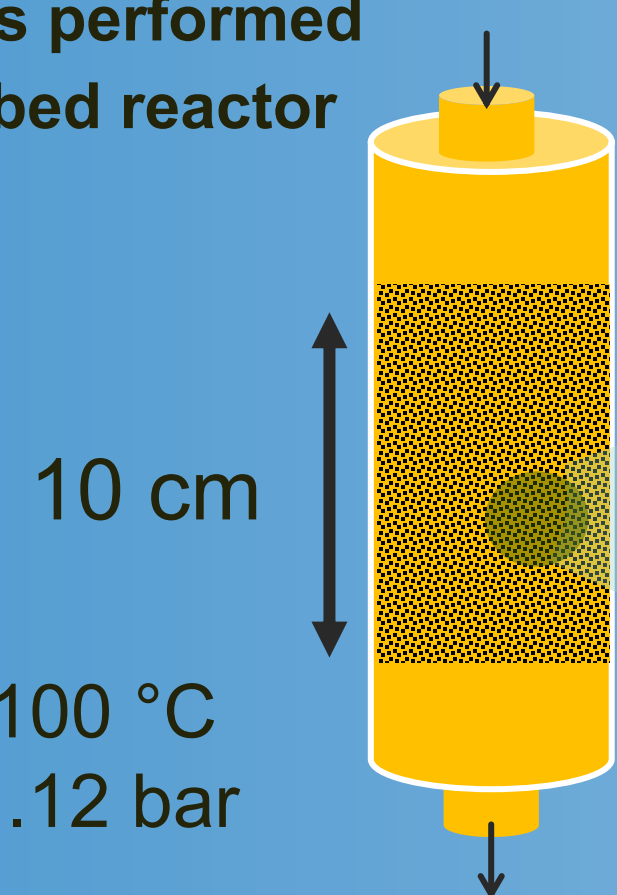
This work addresses the first step, by developing a kinetic model for COS formation over a zeolite 13X catalyst:



METHODOLOGY

Experimental campaign

Experiments performed in a packed-bed reactor



Zeolite 13X

Modeling approach

Reactor modeling

$$\frac{\partial C_i(x,t)}{\partial t} = -\frac{L}{\tau_b} \frac{\partial C_i(x,t)}{\partial x} + \frac{\rho_b}{\varepsilon_b} R_{w,i}$$
$$\frac{\partial L_{i*}(x,t)}{\partial t} = R_{w,i*}$$

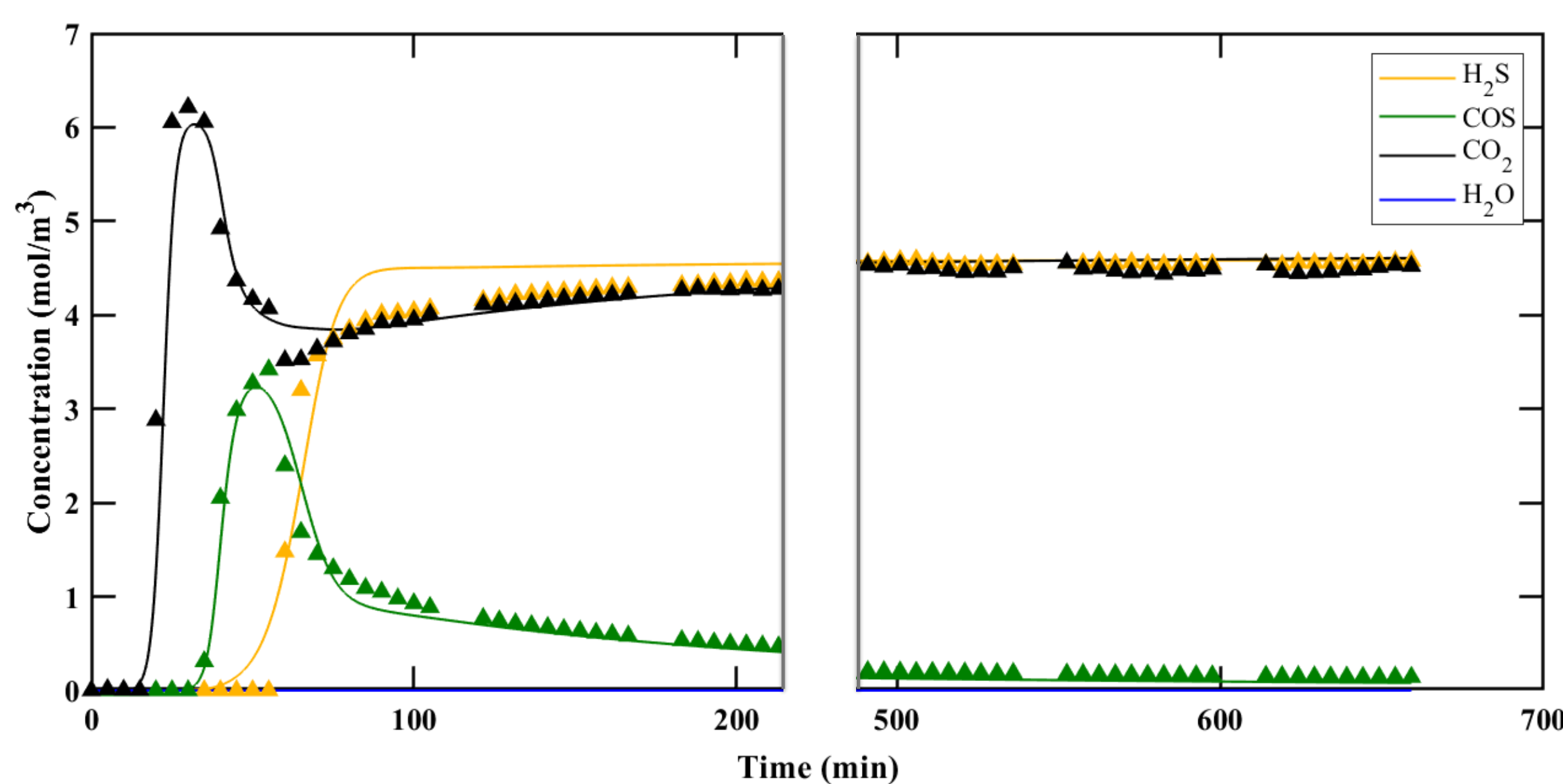
Reaction modeling

Based on the LHHW reaction mechanism	
Reaction equation	Rate equation [mol (kg s) ⁻¹]
$\text{H}_2\text{S} + * \rightleftharpoons \text{H}_2\text{S}^*$	$r_1 = k_{\text{H}_2\text{S}}^+ \left(C_{\text{H}_2\text{S}} L_* - \frac{1}{K_{\text{H}_2\text{S}}^{\text{eq}}} L_{\text{H}_2\text{S}} \right)$
$\text{CO}_2 + * \rightleftharpoons \text{CO}_2^*$	$r_2 = k_{\text{CO}_2}^+ \left(C_{\text{CO}_2} L_* - \frac{1}{K_{\text{CO}_2}^{\text{eq}}} L_{\text{CO}_2} \right)$
$\text{H}_2\text{S}^* + \text{CO}_2^* \rightarrow \text{COS}^* + \text{H}_2\text{O}^*$	$r_3 = k_{\text{r}} L_{\text{CO}_2} L_{\text{H}_2\text{S}}$
$\text{COS} + * \rightleftharpoons \text{COS}^*$	$r_4 = k_{\text{COS}}^+ \left(C_{\text{COS}} L_* - \frac{1}{K_{\text{COS}}^{\text{eq}}} L_{\text{COS}} \right)$

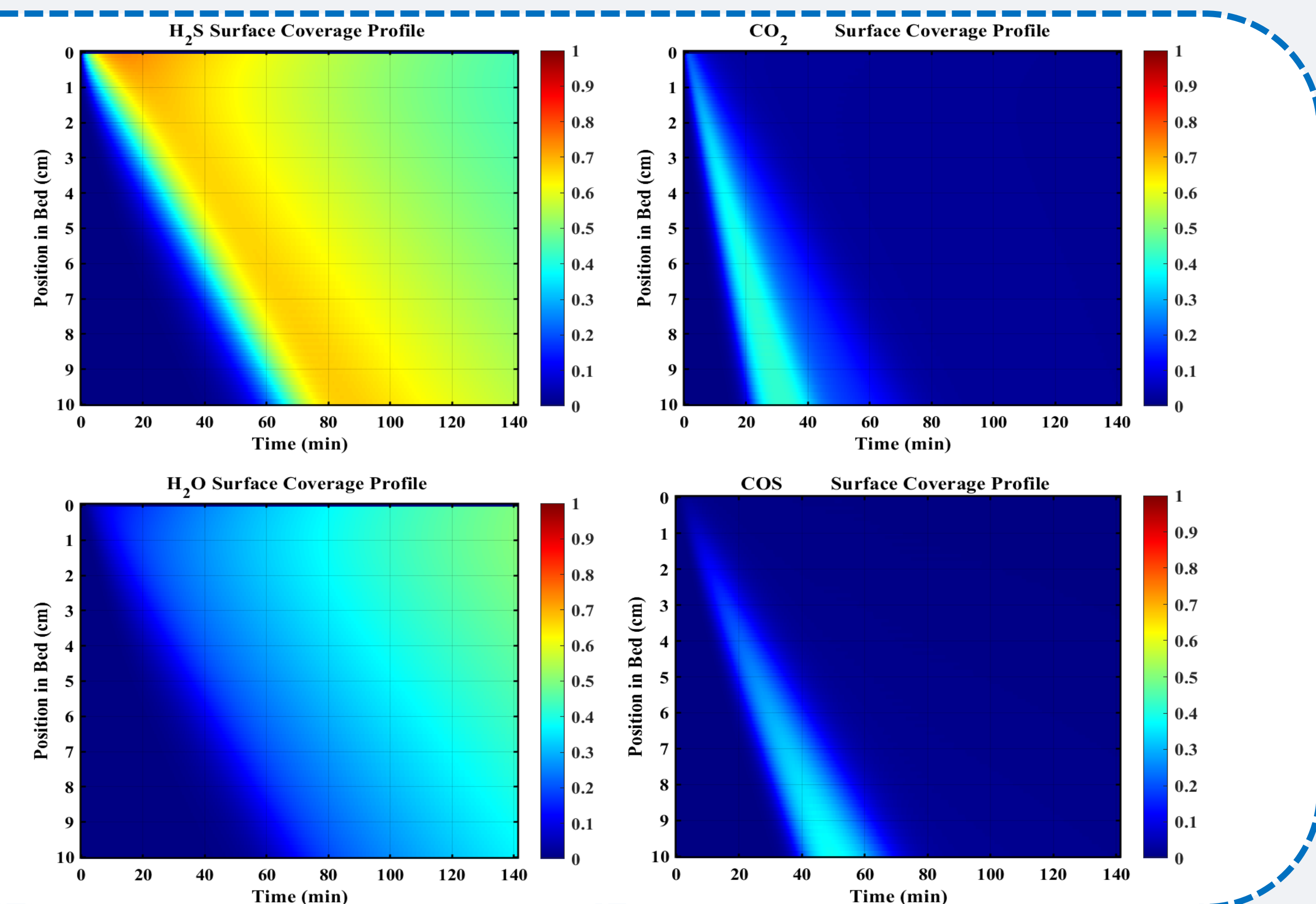
RESULTS AND DISCUSSION

Model fitting

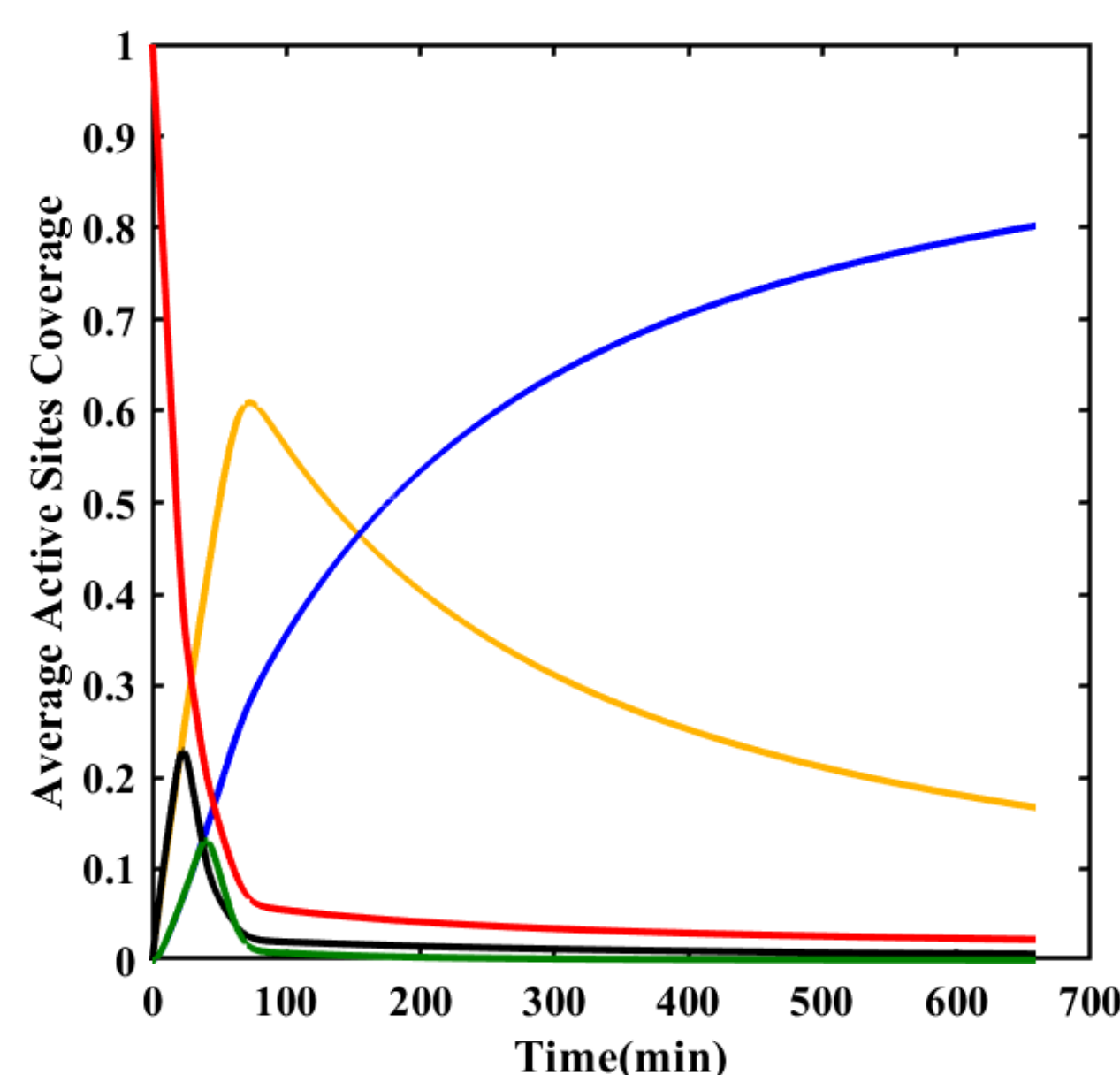
H₂S:CO₂:N₂ (%v/v)
13:13:74



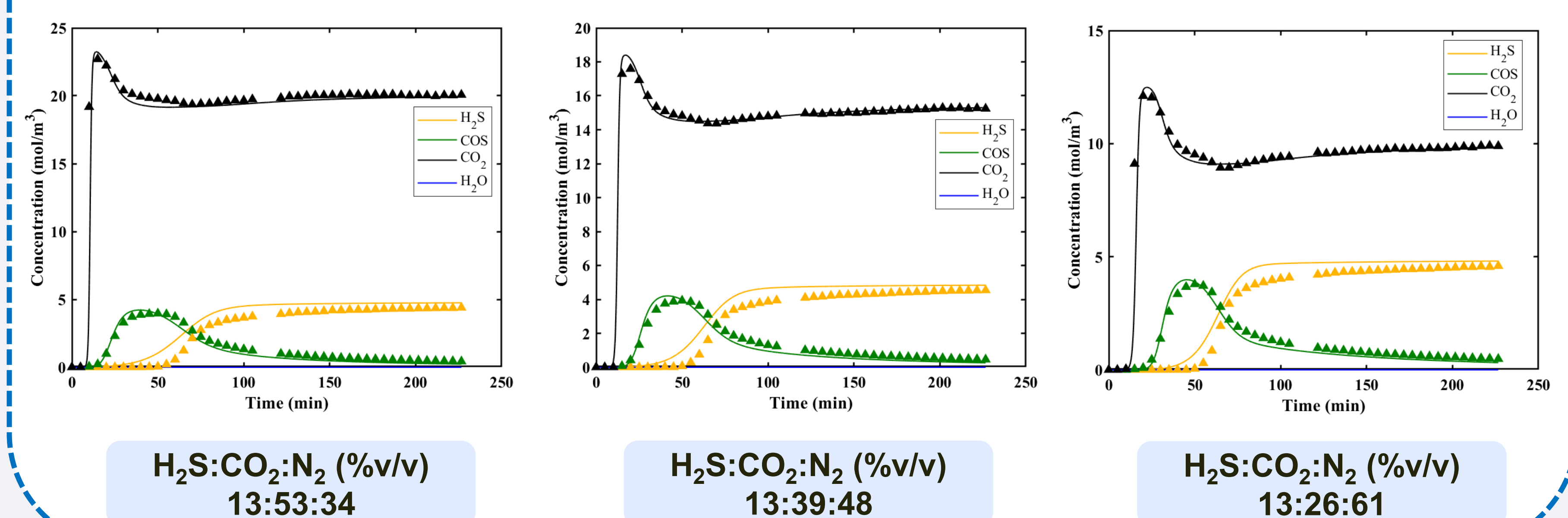
Surface coverage profiles along the reactor bed (y-axis) over time (x-axis).



Model predicted average active site coverages indicate that accumulation of water in the zeolite pore system drives the decline in performance.



Model validation across different feed compositions



CONCLUSIONS

- The elementary-step model revealed the underlying interplay of adsorption, reaction, and catalyst deactivation through water accumulation leading to the experimentally observed trends.
- The model can properly predict experimental results across various feed compositions.

ACKNOWLEDGEMENTS



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