



40th annual meeting of GFZ – international edition
March 31st – April 3rd 2025, Blériot-Plage, France



Acid gas valorisation on Na-Faujasite

Catalytic COS formation

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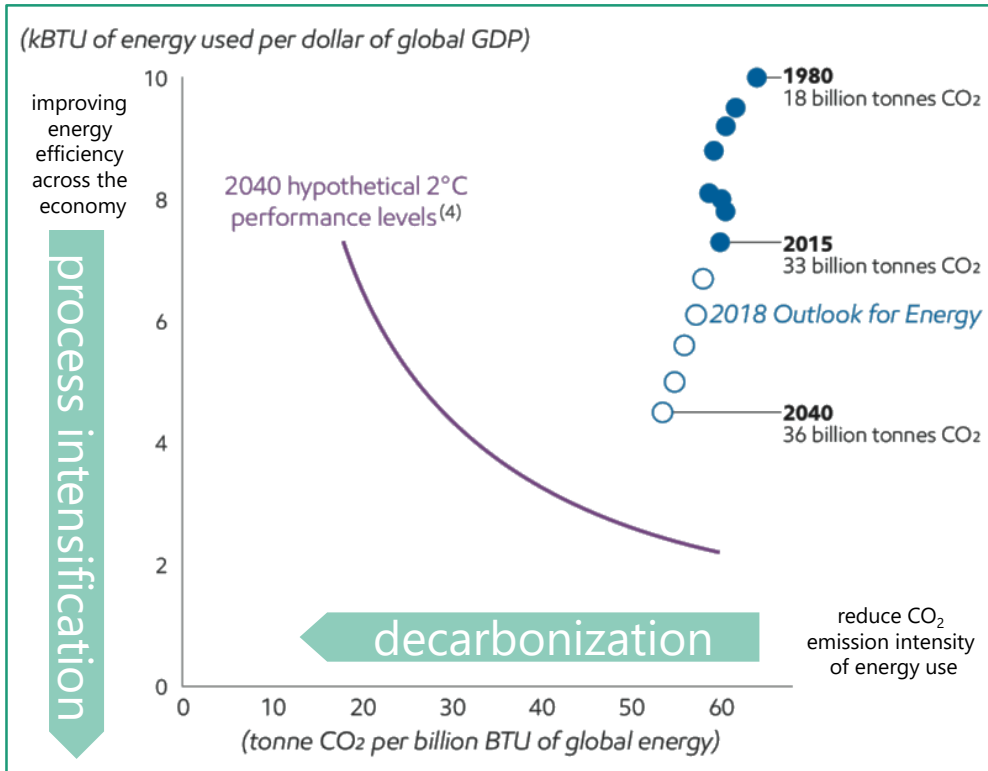
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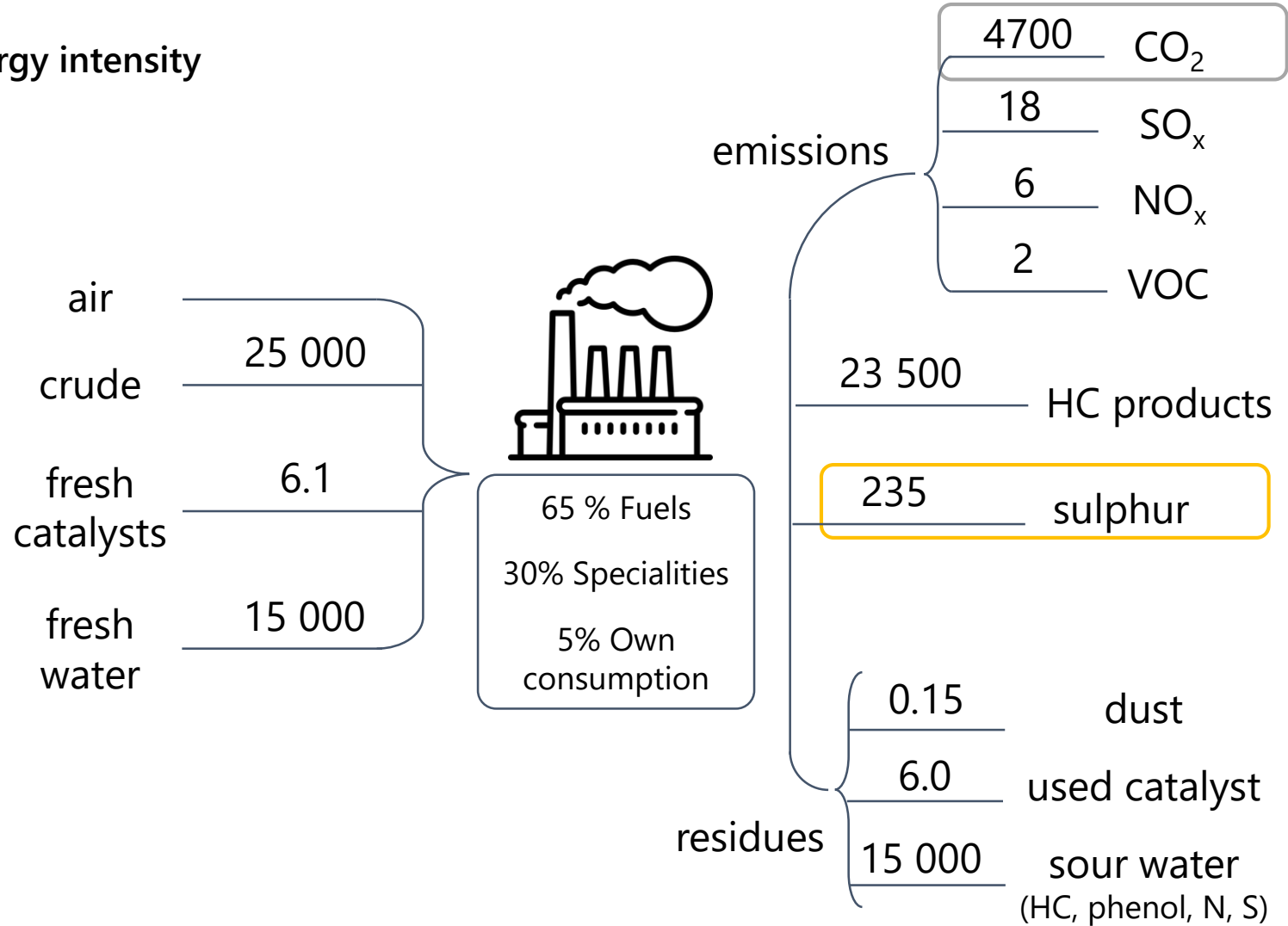


Context : energy outlook

World energy-related CO₂ emissions related to energy intensity vs CO₂ emission intensity



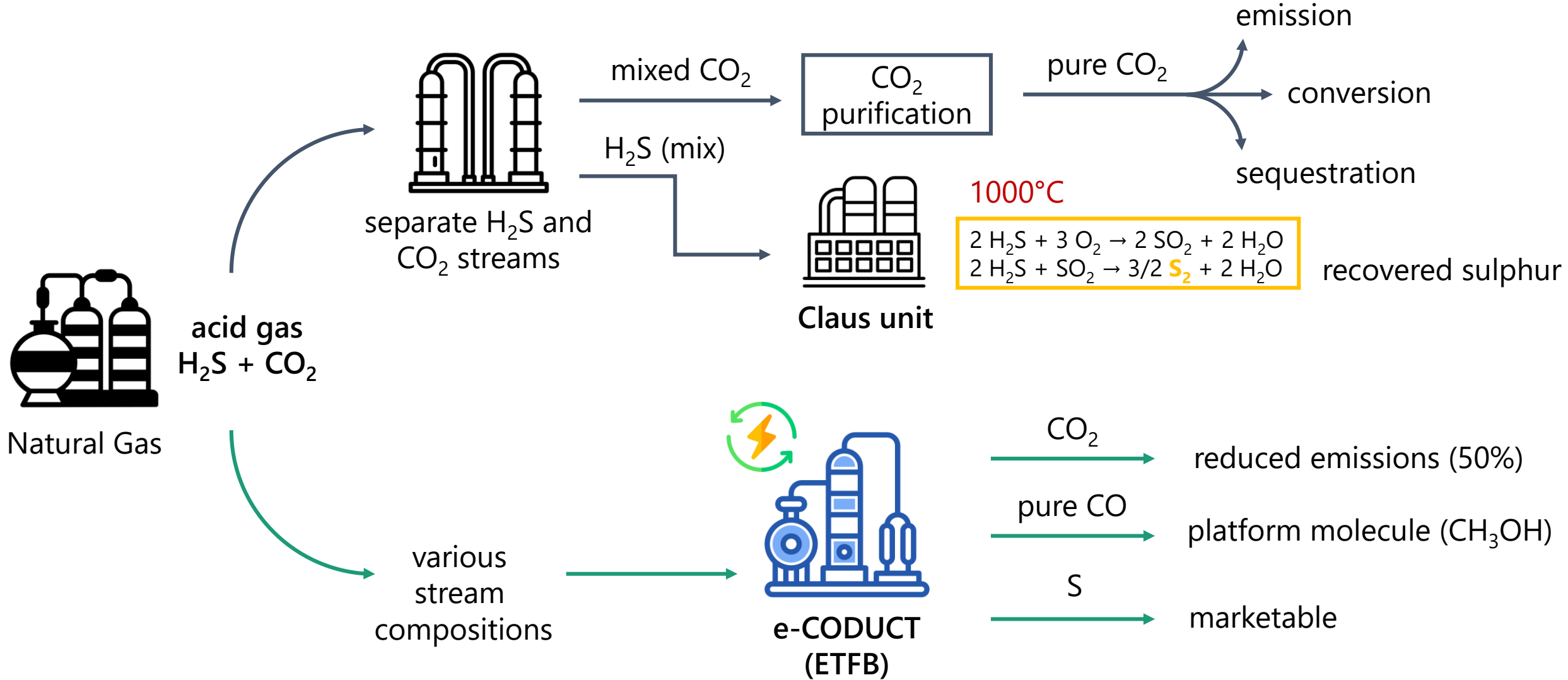
⁽⁴⁾ Based on average Stanford EMF27 full technology / 450ppm scenarios' CO₂ emissions (~20 billion tonnes including energy and industrial processes), ExxonMobil GDP assumptions consistent with 2018 Outlook

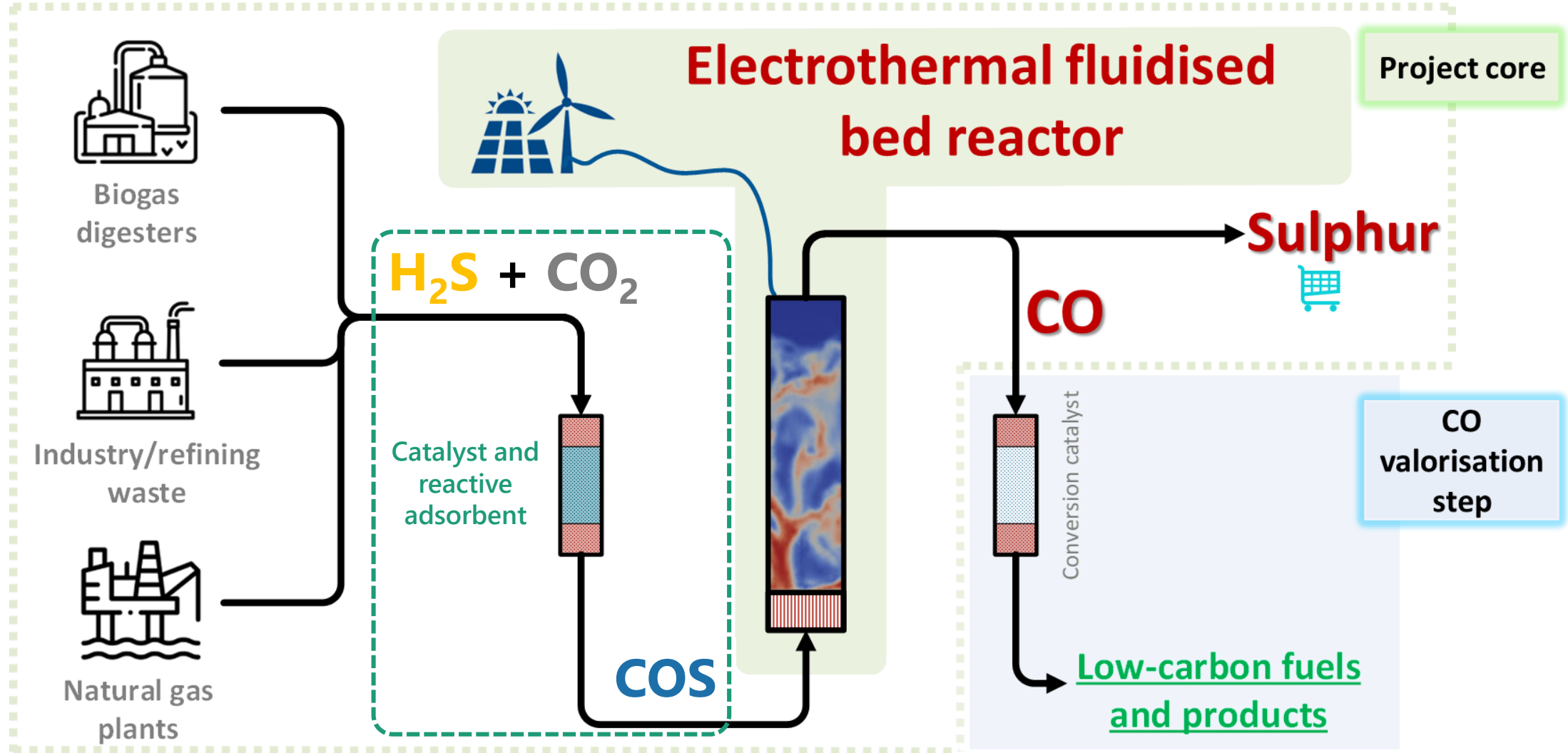


figures are in tonnes per day



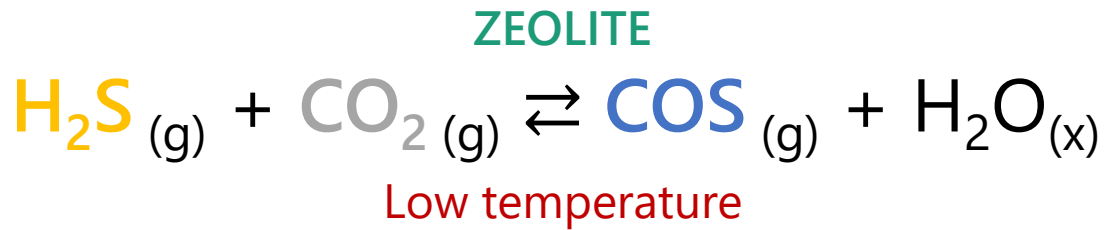
Claus vs COS intermediate





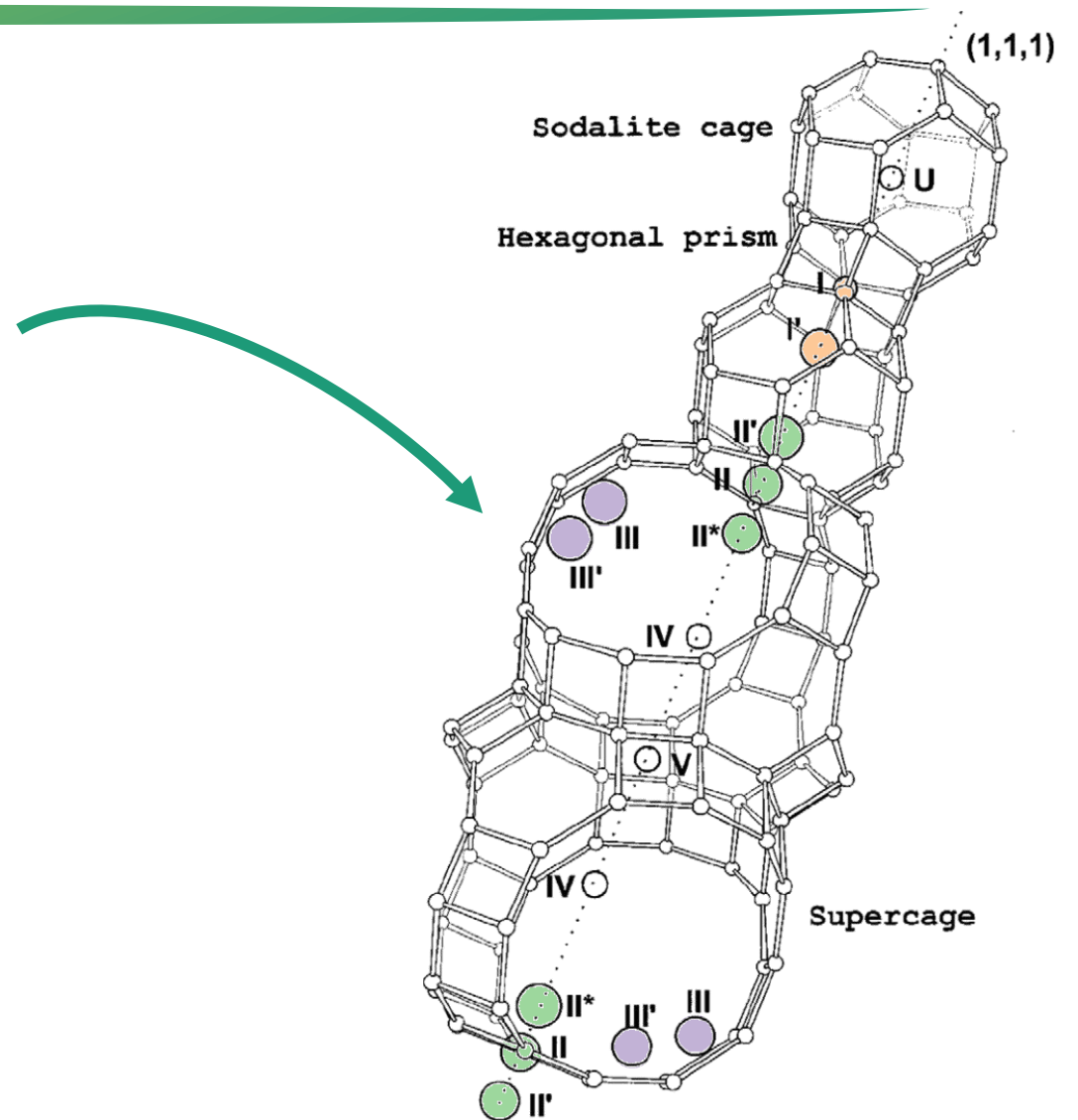


Acid gas conversion on Na-Zeolites



| Water state (x) | gas | adsorbed |
|------------------------------------------------------------|----------|----------|
| $\Delta_r H^0_{298}$ (kJmol ⁻¹) | 31.0 | -11.4 |
| $\Delta_r S^0_{298}$ (JK ⁻¹ mol ⁻¹) | 0 | -118 |
| $\Delta_r G^0_{298}$ (kJmol ⁻¹) | 33.4 | 23.5 |
| Inversion T (K) | ∞ | 199 |
| K eq. (298K) | 1.3E-6 | 7.5E-5 |
| Pressure impact | 0 | ++ |

M. Bülow, *Stud. Surf. Sci. Catal.* 1998

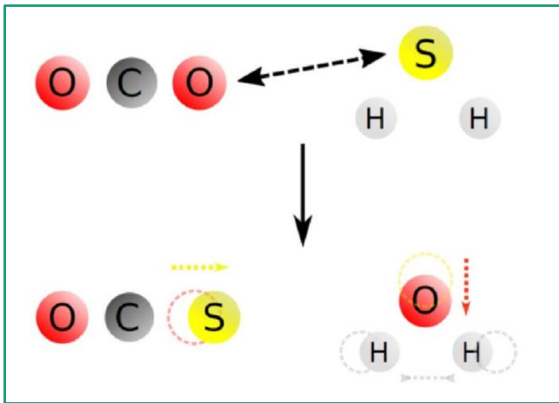


T. Frising, *Microporous Mesoporous Mater.* 2008 5



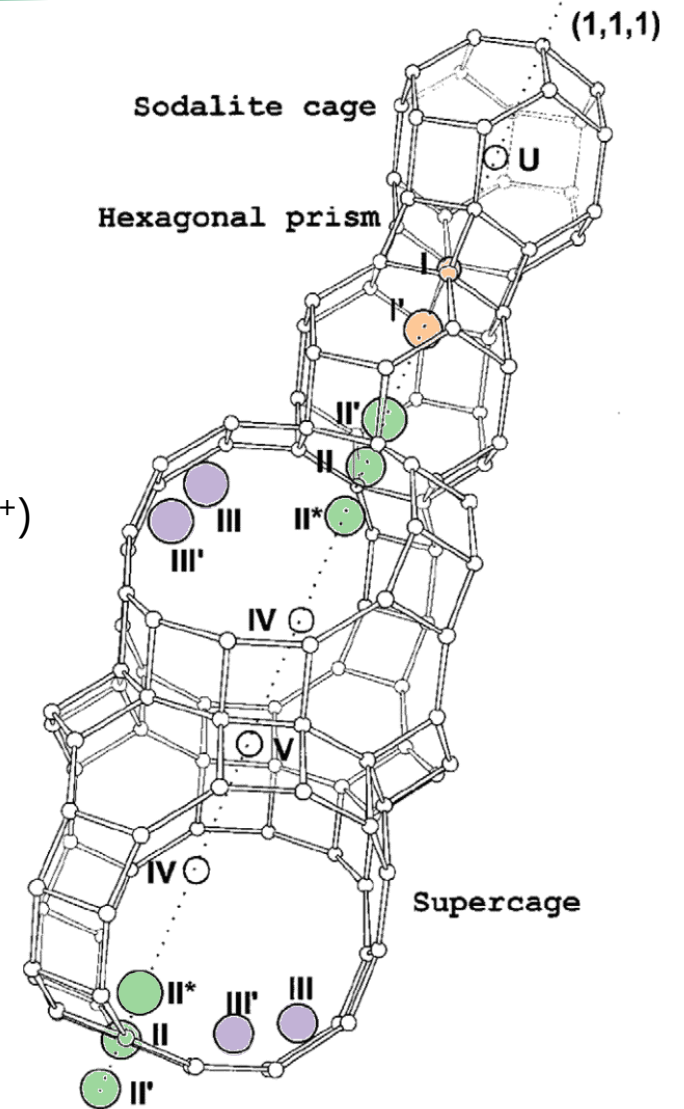
The nature of 13X active site

- Reaction happens on weakly coordinated Na^+ in the α cage
Fellmuth Zeolites 1987
- β cages act as **water sinks** (diffusion controlled, slow kinetics)
W. Lutz Adsorpt. Sci. Technol. 1998
- In NaY ($\text{Si}/\text{Al} > 2.43$) **high water activity** in the α cages (few low coordinated Na^+)
Karge 1978



E. Fetisov, *ChemPhysChem* 2018

- In NaBEA Na^+ pairs yield larger effect on eq. shift than isolated Na
- In NaCaX/A (67-70%) **two sites with different strength** for H_2S dissociative adsorption
A. Starke ACSomega 2022
- H_2S conversion up to 75%
(batch experiment, equimolar to Z capacity)
M. Bülow Stud. Surf. Sci. Catal. 1998



T. Frising, *Microporous Mesoporous Mater.* 2008 6



Conclusions

- Catalytic acid gas conversion to COS at mild temperature tested in **mixed feed and with pre-saturation**
- MKM of both sequences, each one requiring a **dedicated set** of parameters
- The amount of **Na cations accessible to H₂S** is used as the total amount of active sites
- Catalyst **deactivation due to water poisoning** active sites, where *sod* do not participate in water placement even for long reaction times
- Optimization: effect of **temperature**, pressure, etc.



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Thankyou for the kind attention



Merci pour l'attention

